



# A clip-on electroosmotic pump for oscillating flow in microfluidic cell culture devices

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## Abstract

Recent advances in microfluidic devices put a high demand on small, robust and reliable pumps suitable for high-throughput applications. Here we demonstrate a compact, low-cost, directly attachable (clip-on) electroosmotic pump that couples with standard Luer connectors on a microfluidic device. The pump is easy to make and consists of a porous polycarbonate membrane and poly(3,4-ethylenedioxythiophene) polystyrene sulfonate (PEDOT:PSS) electrodes. The soft electrode and membrane materials make it possible to incorporate the pump into a standard syringe filter holder, which in turn can be attached to commercial chips. The pump is less than half the size of the microscope slide used for many commercial lab-on-a-chip devices, meaning that these pumps can be used to control fluid flow in individual reactors in highly parallelized chemistry and biology experiments. Flow rates at various electric current and device dimensions are reported. We demonstrate the feasibility and safety of the pump for biological experiments by exposing endothelial cells to oscillating shear stress (up to 5 dyn/cm<sup>2</sup>) and by controlling the movement of both micro- and macroparticles, generating steady or oscillatory flow rates up to  $\pm 400$   $\mu\text{L}/\text{min}$ .

## 1 Introduction

Microfluidic cell culture devices typically rely on some transport mechanism to drive flow through a cell culture compartment. The transport can be driven through mechanical action, e.g., syringe pumps or peristaltic pumps, or using a nonmechanical technique, such as electroosmosis- or hydrodynamic pressure-based pumps, e.g., pneumatic or gravity-driven pumps. In each of these examples (with a few

exceptions), an off-chip pump or pressure source drives the flow. Generating oscillatory flow requires the pump direction to be periodically reversed or requires sophisticated flow handling with mechanical valves. One of the major benefits of microfluidics is the small quantity of fluid required (pL– $\mu\text{L}$ ), minimizing both cost and waste, particularly with rare reagents such as specially synthesized pharmaceutical candidates. Hence, a pump and its connecting tubing preferably do not require significantly more fluid than the chip it is driving. On the other hand, for cell cultures, a minimum volume of cell culture medium must be present to ensure an isotonic and nutrient-rich environment and provide the sample volumes necessary for chemical analysis (ELISA, HPLC, mass spectrometry, etc.). Off-chip pumps require tubing between the pump and chip, which can lead to “dead volumes” of several mL. Pumps that can handle small volumes with high precision are relatively expensive. Several on-chip pumps reported recently, such as monolithic microfabricated pumps, (Unger et al. 2000) electrochemically actuated pumps, (Suzuki and Yoneyama 2003) and acoustofluidic pumps (Huang et al. 2014), address these issues. These pumps require only minute amounts of fluid and can be directly integrated into the microfluidic device. However, these pumps specialize in delivering low volumes of fluids at low flow rates and are not readily compatible

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Katarina Bengtsson and Jonas Christoffersson have contributed equally to this work.

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with commercial microfluidic devices. To fill this gap, we have created a compact, low-cost, clip-on (attachable) electroosmotic pump that is approximately the same size as a chip (less than half the size of a standard microscope slide), operates at high flow rates without moving parts and without any electric field over the cells in the chip and connects directly to the Luer connector of a microfluidic device without the use of tubing. Furthermore, this electroosmotic pump can be reversed simply by reversing the bias of the applied potential, simplifying the generation of oscillatory flow.

Electroosmotic pumps (EOPs) operate on the principle of electroosmosis, which generates liquid flow through microfluidic channels when an electric field is applied along the channel (Kirby 2010). Electroosmosis is driven by the motion of ions that congregate at the interface between the liquid and the (chemically) charged channel walls. These mobile ions move toward the oppositely charged electrode and, in channels with a diameter  $< 200 \mu\text{m}$ , drag enough fluid with them to create flow. EOPs are usually made in capillaries or chambers filled with porous glass, but can also be made using other porous substrates (Brask et al. 2005; Kwon et al. 2012; Nilsson et al. 2015; Sachan et al. 2014; Snyder et al. 2013). Compared to several other types of pumps, the advantages of EOPs demonstrate a well-controlled (steady or pulsatile) flow, a small footprint and very small dead volume. For cell culture devices, a few EOPs have been demonstrated with cells in suspension (Emmelkamp et al. 2004; Li and Harrison 1997; Xuan and Li 2005). For cells attached to surfaces, examples include the EOP with a concentration gradient generator by Glawdel et al. (2009) and the electroosmotic diode pump with nanoliter precision by Chang et al. (2014). All these EOPs operate at flow rates below a few  $\mu\text{L}$  per minute. To date, relatively few examples of the use of EOPs for cell culture devices can be found, possibly because EOPs operate best at low salt concentration and are therefore not suitable for pumping cell culture medium. Furthermore, operating EOPs with traditional metal electrodes gives rise to water electrolysis and the subsequent generation of  $\text{H}_2$  and  $\text{O}_2$  bubbles and change in pH. These bubbles can disrupt flow, and the pH changes can damage the cells. It has previously been shown that replacing metal electrodes with poly(3,4-ethylenedioxythiophene) polystyrene sulfonate (PEDOT:PSS) electrodes can reduce the amount and impact of water electrolysis in electrokinetic applications (Bengtsson et al. 2014; Bengtsson and Robinson 2017; Erlandsson and Robinson 2011). Further drawbacks of EOPs, as outlined by Byun et al. (2014), include the risk of fouling of the pump by accumulation of, e.g., proteins and cell debris from the medium, as well as electrical damage to the cells in cases where the electrical field is applied over the cell culture to drive the flow.

To overcome these challenges, we have created an EOP that can operate at high flow rates, comparable to other

types of pumps used in microfluidics, without the need to apply an electric field over the cells and with low risk of fouling or causing air bubbles to interfere with the cells. This EOP design can generate high oscillating flow rates with a small dead volume, yielding two advantageous consequences: (1) it provides opportunities to study shear stress effects across the perfused cells, and (2) external metabolites or other excreted molecules can accumulate in the small volumes of a micro-device to reach levels detectable with current analytical methods.

Many cells, such as endothelial cells, cardiac cells, hepatic cells, as well as kidney cells, are affected by shear forces during their differentiation and maturation, motivating the creation of complex shear profiles in microfluidic devices (Esch et al. 2015; Jackman et al. 2016; Jang et al. 2013; Schimek et al. 2013). More specifically, steady shear stress, ranging from 5 to 20  $\text{dyn}/\text{cm}^2$ , has been reported to align endothelial cells in the direction of flow (Li et al. 2005; Schimek et al. 2013) and tighten intercellular connections, which has been used to mimic the tight barrier between the blood and the brain (Booth and Kim 2012). However, compared to steady flow, alternating flow (in which the flow direction is repeatedly reversed) does not cause cell alignment, but, like steady flow, influences cell physiology and gene expression (Deguchi et al. 2005; Franzoni et al. 2016). Oscillatory flow of about  $\pm 4 \text{ dyn}/\text{cm}^2$  occurs at branches in blood vessels and seems to play a key role in the development of atherosclerosis (Davies et al. 2013; Malek et al. 1999). In addition to creating a physiologically relevant environment, oscillating flow (shear) allows the volume of fluid exposed to the cells to be minimized, making it possible to concentrate the minute amounts of biomarkers excreted by the cells, making them easier to identify and quantify.

In this paper, we demonstrate a clip-on (no tubing) electroosmotic pump that generates flow rates up to 400  $\mu\text{L}/\text{min}$ . We have combined advantages of an off-chip pump that handles large volumes (1–2 mL) with the compact size and proximity of an on-chip pump by placing our pump directly on top of the chip. The pump is the size of a syringe filter holder, with integrated PEDOT:PSS electrodes separated by a porous polycarbonate membrane and connected to the chip via a 1-mL syringe. The syringe separates the cell culture medium in the chip from the electrolyte in the pump and allows the flow to be viewed and tracked during this characterization, but could be eliminated or redesigned to reduce the dead volume even further. To test the function of the pump, we used it with two differently sized microfluidic devices to control the motion of both micro- and macroscale particles, as well as for stimulating endothelial cells exerting them to shear stress of about  $\pm 5 \text{ dyn}/\text{cm}^2$  at 0.1 Hz.

## 2 Experimental

### 2.1 Electroosmotic pump

The design of the pump and the microfluidic setup is shown together in Fig. 1. The pump consisted of a hydrophilic polycarbonate membrane (IpPore™, pore diameter 0.2 μm, diameter 25 mm,  $5 \times 10^8$  pores/cm<sup>2</sup>) placed between two poly(3,4-ethylenedioxythiophene) electrodes, each mechanically supported by a loosely woven nylon textile. This stack was placed in a 25-mm membrane syringe filter holder (Sartorius). To allow electrical connection, a 5-mm-wide strip of each electrode exited the filter holder where the threads had been removed to prevent tearing of the electrode during assembly. To protect the electrode strip that passes through the threads of the filter holder and minimize the fluid that “leaks” through the material, this strip was coated with a conducting carbon paste (Leit C Conducting Carbon Cement, Neubauer Chemikalien), followed by melted paraffin wax and a layer of vacuum grease (High vacuum grease, Dow Corning®).

The electrodes were prepared by applying 0.1–0.2 g/cm<sup>2</sup> (wet) PEDOT:PSS on the nylon textile. These were then baked at 50 °C for 2 h, followed by a temperature ramp of 3.6 °C h<sup>-1</sup> to 90 °C, finishing with 90 °C for 5 h. After cooling to room temperature, the electrodes were rinsed in 0.1 M NaCl for 16 h and neutralized (to pH ~ 7) using 0.1 M NaOH before assembly with the membrane in the syringe filter holder.

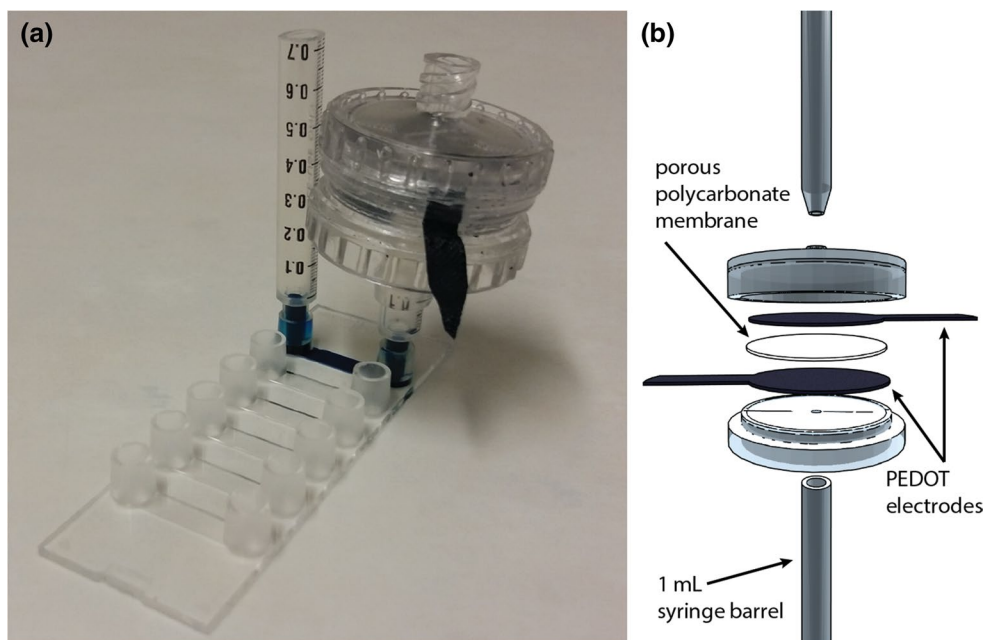
### 2.2 Cell culture

Human umbilical vein endothelial cells (HUVECs, ThermoFisher) were used at passage 3 or 4 and cultured in Medium 200 (ThermoFisher) supplemented with low serum growth supplement (LSGS, ThermoFisher). For flow experiments, the cells were trypsinized, centrifuged and resuspended in cell culture medium at a concentration of  $15 \times 10^6$  cells/mL. To minimize the risk of air bubble formation in the channels, the microfluidic slides and cell culture medium were both incubated at 37 °C overnight. The cells were seeded in pre-coated microfluidic channels (μ-slide VI<sup>0.1</sup>, IbiTreat, Ibidi) using a 1-mL syringe and were allowed to attach for at least 2 h before new cell culture medium was added to the reservoirs of the slide. If the slides were not used for flow experiments the same day, they were placed on a rocking platform to stir the culture medium. Live/Dead assays were performed using calcein and ethidium homodimer-1 (both from LifeTechnologies) and Hoechst 33,342 (ThermoFisher) to stain the nuclei. The cells were visualized in a confocal microscope (Zeiss Axio Observer.Z1, LSM700). Images were processed using ImageJ software (NIH).

### 2.3 Flow experiments

One-microliter syringes were attached to microfluidic channels with height of 100 μm (cross-sectional area 0.1 mm<sup>2</sup>, μ-Slide VI<sup>0.1</sup>) and seeded with HUVECs or microparticles (20 μm, microparticles GMBH), or a height of 400 μm (cross-sectional area 1.52 mm<sup>2</sup>, μ-Slide VI<sup>0.4</sup>, untreated, Ibidi) and filled with microparticles (20 μm, microparticles

**Fig. 1** Pump and cell culture chip assembly. **a** Photograph of the electroosmotic pump incorporated into a modified syringe filter holder and connected onto a microfluidic device filled with blue dye. The syringe barrel on the left side of the channel was used to balance the hydrostatic pressure. **b** Exploded schematic of the pump in a modified syringe filter holder. The electroosmotic pump consisted of a track-etched polycarbonate membrane sandwiched by two PEDOT:PSS electrodes (color figure online)



GMBH), or macroparticles (100  $\mu\text{m}$ , CultiSpher<sup>TM</sup>, Percell Biolytica). All equipment was either acquired sterile or rinsed in ethanol prior to use. The pump was connected to a shortened syringe holding a volume of about 200  $\mu\text{L}$  and contained a bubble of approximately 100  $\mu\text{L}$  to separate the buffer in the pump (1 mM TrisHCl, Trizma<sup>®</sup> base, Sigma, pH 7) from the cell culture medium in the chip and allow the displacement of fluid to be easily monitored. Note that this, relatively large, additional piece is only necessary when calibrating the pump. Normally the pump can be placed directly on the chip, and the bubble separating the fluids can reside in the Luer connector. The assembly was placed on a microscope heating insert (37  $^{\circ}\text{C}$ ) on top of a microscope (SVM340, Labsmith). Before starting the pump, the levels in the two syringe reservoirs were adjusted until there was no visible pressure-driven flow through the fluidic channel. The motion of the bubble in the syringe connected to the pump was tracked using a camera (DinoLite Pro), allowing the flow rate to be estimated during the experiment and carefully analyzed afterwards. The videos recorded were used to determine the vertical position of the center and edge of the top meniscus, using MATLAB, with an estimated accuracy of about 0.1 mm (2  $\mu\text{L}$ ). These data were used to calculate the volumetric flow rate and pressure drop over the meniscus interface.

## 2.4 Image analysis and statistics

To better visualize the cell morphology in the Live/Dead assay, the green channel (showing cell cytosol) was convoluted with a  $5 \times 5$  high-pass filter. The mean and SD of the area and shape index of 150 cell nuclei, and the cell surface coverage at three locations, were measured using ImageJ. The shape index indicates the circularity of the nucleus, where the maximum 1 represents a perfect circle. Differences in the populations were analyzed by the nonparametric Mann–Whitney test for area and Student's  $t$  test for shape index and the surface coverage, and considered significant for  $p < 0.01$ .

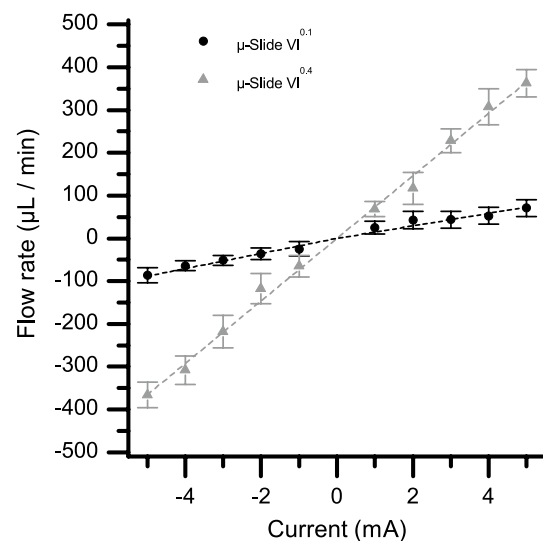
## 3 Results and discussion

### 3.1 Design and performance of the electroosmotic pump

The pump was designed to easily connect to commercial microfluidic devices and operate at high flow rates. Furthermore, it was designed to overcome previously reported limitations of EOPs: electrolysis of water at high voltages, risk of electrical damage to cells, fouling of the membrane by impurities from the pump fluid or cell culture medium, and

poor performance with the salt concentration of cell culture medium (Byun et al. 2014).

These criteria resulted in a design for an EOP integrated onto the Luer connector of a commercially available microfluidic channel (Fig. 1). A porous polycarbonate membrane was sandwiched between two pieces of PEDOT:PSS-coated nylon fabric. Each pore in the membrane functions as an EOP, i.e., the volumetric flow rate is proportional to the pore density. The flexibility of the polycarbonate membrane, the nylon fabric and the polymer used in the electrodes allowed the incorporation of the pump into a syringe filter holder with access to one electrode on each side. To separate the cell culture medium from the pump solution, approximately 100  $\mu\text{L}$  of air was drawn into the syringe that connected the pump to the Luer coupling on the chip. On the other side of the channel, medium is placed in a second syringe to balance gravity-induced pressure. The flow generated by the pump is quantified in Fig. 2. A maximum flow rate of  $\sim 400 \mu\text{L}/\text{min}$  at  $\pm 5 \text{ mA}$  was achieved when the resistance to flow was minimized, i.e., the pump was connected to the  $\mu\text{-Slide VI}^{0.4}$ , compared to a maximum flow rate of  $\sim 90 \mu\text{L}/\text{min}$  at  $\pm 5 \text{ mA}$  when connected to the  $\mu\text{-Slide VI}^{0.1}$ . When operated at  $\pm 5 \text{ mA}$ , the applied potential reached a maximum of about 2.5 V, making the peak power consumption about 13 mW. The electroosmotic mobility  $\mu_{\text{eo}}$  was estimated by linear regression of flow velocity versus the mean applied potential, resulting in  $\mu_{\text{eo}} = (3.86 \pm 0.22) \times 10^{-10} \text{ m}^2/\text{V s}$ , similar to what has been measured during previous characterization of the membrane-based pumping setup (Bengtsson and Robinson 2017). This value corresponds to



**Fig. 2** Average volumetric flow rate ( $N = 3$ ) versus current for two different configurations: connected to a  $\mu\text{-Slide VI}^{0.4}$  (gray triangles) and connected to a  $\mu\text{-Slide VI}^{0.1}$  (black circles), pumping 1 mM TrisHCl, (pH  $7.1 \pm 0.1$ ) in each case. Dashed lines represent linear fits (through the origin) of each data set. Error bars indicate  $\pm 1$  SD

a  $\zeta$  potential of  $-0.55 \pm 0.03$  mV, calculated according to  $\zeta = -u_{\text{eo}}\eta/(\epsilon_r\epsilon_0)$  where the solution viscosity  $\eta = 1.01$  cP (Haynes et al. 2015) and the relative dielectric constant  $\epsilon_r = 80$  (Kirby 2010; Nörtemann et al. 1997). We estimate (but did not measure) a maximum hydrostatic pressure (at zero flow) to be approximately 100 mm H<sub>2</sub>O per V of applied potential based on our previous pump characterization (Bengtsson and Robinson 2017) with a similar pump membrane that had double the pore diameter and a maximum pressure of 25 mmH<sub>2</sub>O/V. (Halving the diameter theoretically increases the maximum pressure 4 $\times$ .) The pressure drop across the top meniscus of the bubble in the syringe was estimated from the meniscus curvature and surface tension of the air–water interface to be at most 70 Pa.

The oscillatory flow of the pump was also verified using micro- and macroparticles (20 and 100  $\mu\text{m}$  in diameter, respectively) under oscillation between 0.1 and 0.25 Hz, see Supplementary information videos 1 and 2. The maximum microparticle velocity corresponded to a volumetric flow rate of 100  $\mu\text{L}/\text{min}$  at  $\pm 5$  mA in the  $\mu\text{-Slide VI}^{0.1}$ .

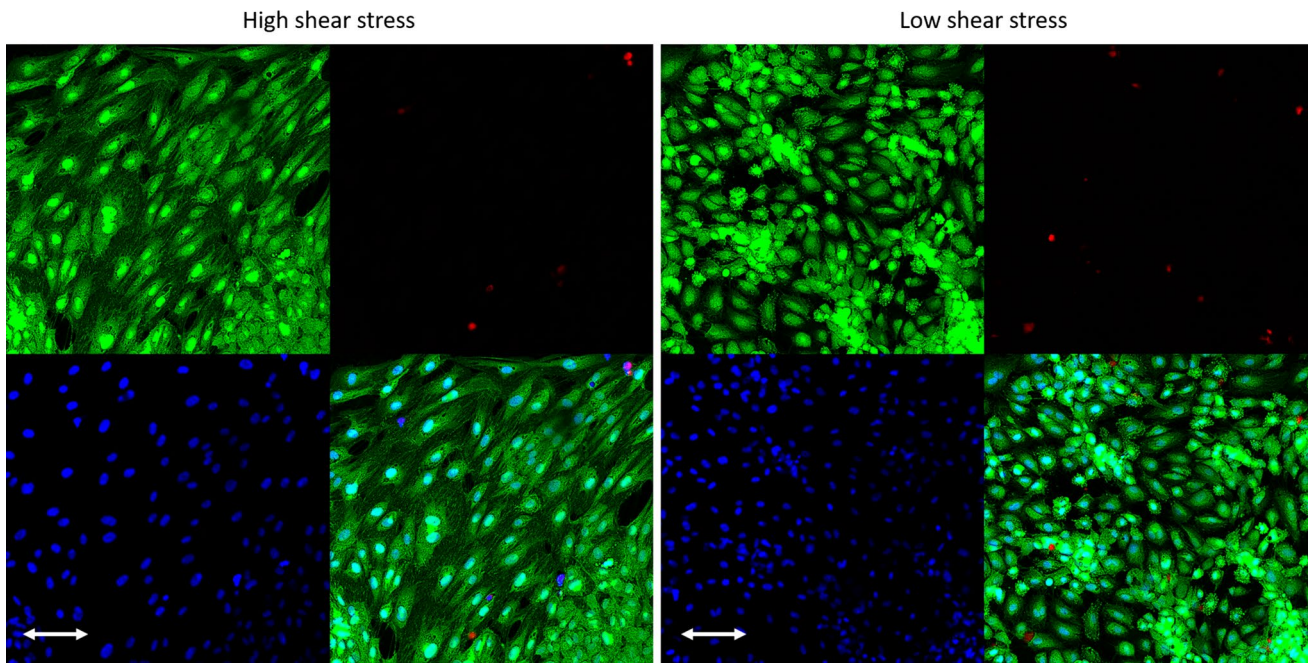
The pump initially generated a flow rate of 90  $\mu\text{L}/\text{min}$ , but stabilized at 60  $\mu\text{L}/\text{min}$  within 16 h with consistent flow rates over the next 48 h at  $\pm 5$  mA. The decreasing flow rate was probably caused by decreasing pH in the pump electrolyte. The electrolyte in the pump started with a pH of 7, and for the instances when the flow rate decreased, the pH was found to be between 4.8 and 5.8 after the experiment. The pH changes may have been caused by water electrolysis or leeching of H<sup>+</sup> from the PEDOT:PSS electrodes. The generation of pH changes by water electrolysis in the pump electrolyte can be reduced by increasing the mass (thickness), and concomitantly the columbic capacity, of the polymer used in the electrodes. The leeching of protons from the PSS in the electrodes can be minimized via electrochemical ion exchange before assembly, or through continued operation in the pump (as long as the pump electrolyte is replaced). The impact of either mechanism can likely be reduced by decreasing the initial pH of the pump electrolyte and/or adding pH buffer to the electrolyte. Replacing the electrolyte in the pump restored the pump's performance, increasing the flow rate to the starting value. This implies that the flow rate could be further increased by increasing the pH of the electrolyte in the pump and shows the importance of minimizing electrolysis in the pump. No decrease in flow rate was observed during the calibration measurements taken to collect the data in Fig. 2, which only took about an hour. Modifying or replacing the porous polycarbonate membrane in this pump could increase the volumetric flow rate, e.g., through increasing the porosity of the membrane or increasing the surface charge density.

By separating the pump electrolyte from the cell media in the chip, we eliminated the risk of any electrolytic byproducts or residue from the PEDOT:PSS electrodes contacting

the cells. The separate electrolyte also allowed us to use a low (nonphysiological) concentration of salt in the pump, increasing the pump's performance and reducing the risk of clogging of the membrane with cell proteins and debris.

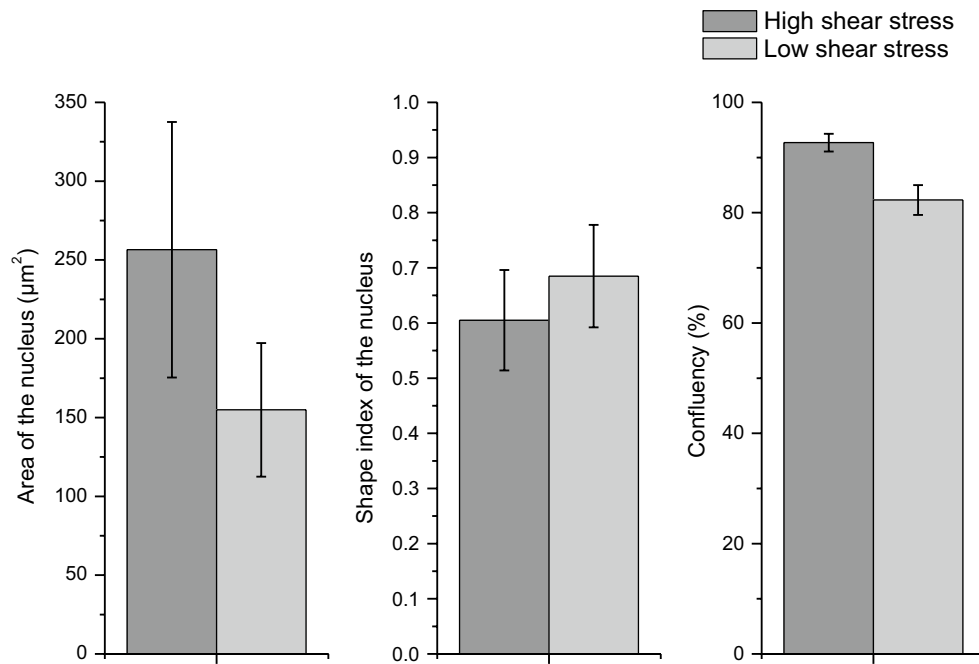
### 3.2 Inducing shear stress on endothelial cells with the pump

To investigate the performance and compatibility of the EOP with cultured cells, human endothelial cells (HUVECs) were exposed to oscillating flow generated by the pump. As described previously, these cells were expected to respond to shear stress. We hypothesized that the EOP would produce a sufficient flow to induce a physiological change in the cells. Based on previously reported shear stress studies on in vivo veins, and reports of shear stress used to induce morphological changes in endothelial cells, we aimed to achieve a shear stress of at least  $\pm 5$  dyn/cm<sup>2</sup> (Malek et al. 1999; Schimek et al. 2013). The HUVECs were seeded in microfluidic channels and exposed to an alternating shear stress of at least  $\pm 5$  dyn/cm<sup>2</sup> (high shear,  $\sim 60$   $\mu\text{L}/\text{min}$ ) or  $\pm 2.2$  dyn/cm<sup>2</sup> (low shear,  $\sim 25$   $\mu\text{L}/\text{min}$ ) by driving currents at  $\pm 5$  or  $\pm 2$  mA, respectively, for 5 s in each direction (0.1 Hz). As previously explained, the flow rate generated by driving the pump at  $\pm 5$  mA started at  $\sim 90$   $\mu\text{L}/\text{min}$  or  $\pm 7$  dyn/cm<sup>2</sup>, but decreased over time before stabilizing at 60  $\mu\text{L}/\text{min}$  within 16 h. No decrease in flow rate over time was observed when driving the flow at  $\pm 2$  mA. The viability of the cells after 48 h of pumping was confirmed with a Live/Dead assay (Fig. 3). As expected, the endothelial cells did not align in the direction of the oscillatory flow (see Fig. 3 and supplementary video 3). However, the mean area and shape index of the cell nuclei and the total cell coverage were all statistically different between cells exposed to high (5 dyn/cm<sup>2</sup>) and low (2.2 dyn/cm<sup>2</sup>) oscillating shear (see Fig. 4). Morphological changes in the cell nucleus area and decreased permeability due to an increased membrane integrity have previously been attributed to shear stress from laminar flow on endothelial cells (Booth and Kim 2012; Deguchi et al. 2005). Furthermore, the high level of oscillatory shear appears to induce enlargement and stretching of the cells, as well as a decrease in the number of nuclei, as shown in Fig. 3. This has previously been explained by a decrease in the growth rate of endothelial cells due to high shear stress (Li et al. 2005; Malek et al. 1999). Consequently, fewer cells occupy the same area and can therefore become larger and potentially also elongated.



**Fig. 3** Live/Dead assay after 48 h of alternating flow at  $\pm 5 \text{ dyn/cm}^2$  (high shear, left) and at  $\pm 2.2 \text{ dyn/cm}^2$  (low shear, right) showing living cells in green, dead cells in red, and cell nuclei in blue, each

through a 10 $\times$  objective. Each color channel is shown separately, and then as a composite (bottom right). The arrow indicates the direction of the oscillating flow and a length of 100  $\mu\text{m}$  (color figure online)



**Fig. 4** Mean and SD cell nucleus area, shape index, and cell surface coverage (confluency) for cells exposed to low ( $\pm 2.2 \text{ dyn/cm}^2$ ) and high ( $\pm 5 \text{ dyn/cm}^2$ ) alternating shear. The high shear stress signifi-

cantly affected the cell nucleus morphology (area and shape of the nucleus) and the confluency

## 4 Conclusion

The broad adoption of highly parallelized chemical and biological flow experiments for applications such as pharmaceutical testing has, in part, been limited by the need for external appliances such as pumps. When designing such a system, one must typically choose between on-chip pumps, which require the fabrication of relatively expensive, highly specialized chips, and remote pumps that must be connected via tubing and dramatically increase the volume of each flow circuit. For practical and commercial reasons, the entire fluidic setup surrounding microfluidic devices should be well integrated into the device and the various operative components such as pumps and detectors should be approximately the same size as the chip itself. Ideally, the fluidic setup should be able to provide a wide range of flow rates while minimizing the volume of liquid, and the quantity of costly pharmaceuticals, required.

In this paper, we have presented an oscillating electroosmotic pump that fits onto connectors typical of commercially available microfluidic chips. The pump, which is less than half the size of the chip used in this study, was able to drive cell medium at flow rates up to 400  $\mu\text{L}/\text{min}$  through a microfluidic channel with a cross-sectional area of 1.52  $\text{mm}^2$ , and up to 90  $\mu\text{L}/\text{min}$  through an area of 0.1  $\text{mm}^2$ . These volumetric flow rates were sufficient to induce an apparent morphological response of endothelial cells by exposing them to an alternating shear stress of  $\pm 5 \text{ dyn}/\text{cm}^2$  for 48 h. The pump delivered reproducible flow rates and maintained the cells for over 96 h. These performance properties make the EOP a viable alternative for a variety of microfluidic configurations.

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## Compliance with ethical standards

**Conflict of interest** NDR and KB have a stake in LunaMicro AB, which owns a patent protecting the use of electrochemically active electrodes in electrokinetic devices.

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